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**TITLE: METHOD AND APPARATUS FOR HUMIDIFICATION AND
TEMPERATURE CONTROL OF INCOMING FUEL CELL PROCESS GAS**

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Title: METHANOL AND APPARATUS FOR HUMIDIFICATION AND
TEMPERATURE CONTROL OF INCOMING FUEL CELL PROCESS
GAS

5 FIELD OF THE INVENTION

The present invention relates generally to a method and apparatus for humidifying and controlling the temperature of incoming fuel cell process gas. More particularly, the present invention relates to a humidification system capable of providing rapid, accurate and precise control of both the relative humidity and the temperature of the incoming fuel cell process gas.

BACKGROUND OF THE INVENTION

Fuel cell systems are seen as a promising alternative to traditional power generation technologies due to their low emissions, high efficiency and ease of operation. Fuel cells operate to convert chemical energy into electrical energy. Proton exchange membrane fuel cells comprise an anode, a cathode, and a selective electrolytic membrane disposed between the two electrodes. In a catalyzed reaction, a fuel such as hydrogen, is oxidized at the anode to form cations (protons) and electrons. The ion exchange membrane facilitates the migration of protons from the anode to the cathode. The electrons cannot pass through the membrane and are forced to flow through an external circuit thus providing an electrical current. At the cathode, oxygen reacts at the catalyst layer, with electrons returned from the electrical circuit, to form anions. The anions formed at the cathode react with the protons that have crossed the membrane to form liquid water as the reaction product.

Proton exchange membranes require a wet surface to facilitate the conduction of protons from the anode to the cathode, and otherwise to maintain the membranes electrically conductive. It has been suggested that each proton that moves through the membrane drags at least two or three water molecules with it (U.S. Patent 5,996,976). U.S. Patent 5,786,104 describes in more qualitative terms a mechanism termed "water pumping", which results in the transport of cations (protons) with water molecules through the membrane. As the current density increases, the number of

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water molecules moved through the membrane also increases. Eventually the flux of water being pulled through the membrane by the proton flux exceeds the rate at which water is replenished by diffusion. At this point the membrane begins to dry out, at least on the anode side, and its internal resistance increases. It will be appreciated that this mechanism drives water to the cathode side, and additionally the water created by reaction is formed at the cathode side. Nonetheless, it is possible for the flow of gas across the cathode side to be sufficient to remove this water, resulting in drying out on the cathode side as well. Accordingly, the surface of the membrane must remain moist at all times. Therefore, to ensure adequate efficiency, the process gases must have, on entering the fuel cell, a predetermined or set relative humidity and a predetermined or set temperature which are based on the system requirements.

A further consideration is that there is an increasing interest in using fuel cells in transport and like applications, e.g. as the basic power source for cars, buses and even larger vehicles. As compared to some stationary applications, this presents some unique requirements. More particularly, it is necessary that the power delivered by a fuel cell be capable of rapid change between different power levels, and these power levels can be quite different. Thus, in urban driving, it is common for fuel cells to be required to frequently switch between minimum, or even zero power, to a maximum power level and back again. Maintaining appropriate humidity levels under such severe operating conditions is not easy. Additionally, a fuel cell must be capable of providing this functionality under a wide range of ambient air conditions.

Accordingly, in this art one can find numerous proposals for maintaining humidity in fuel cell systems. One conventional way to humidify a gas stream is to pass a gas as a stream of fine bubbles through water. As long as the process gas has sufficient contact time with the water, controlling the temperature of the water controls the amount of water in the gas stream. However, these bubble column type humidifiers are generally not suitable for fuel cells. The humidifiers tend to be large and costly. Moreover, the humidifiers are unable to react fast enough to meet the load following requirements of the fuel cell system. As a result, at high gas flow

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(c) removing excess condensed water from the process gas stream; and

(d) heating the process gas stream until it reaches a third pre-set temperature.

5 In one embodiment, the method further comprises the step of maintaining the third pre-set temperature of the process gas stream from step (d) until it reaches an inlet of a fuel cell.

In accordance with another embodiment of the present invention, there is provided an apparatus for humidifying a process gas stream for an operating fuel cell, the apparatus comprising:

10 (a) a means for super-saturating and heating the process gas stream with steam until it reaches a first pre-set temperature;

(b) a means for cooling the process gas stream until it reaches a second pre set temperature;

15 (c) a means for removing excess condensed water from the process gas stream; and

(d) a means for heating the process gas stream until it reaches a third pre-set temperature.

20 In one embodiment, the apparatus further comprises a means for maintaining the third pre-set temperature of the process gas stream from step (d) until it reaches an inlet of a fuel cell.

The present invention has many advantages over the prior art. The combination of the dewpoint cooling section and reheating section allows rapid changes in operating conditions, with response times that are less than 30 seconds. Furthermore, the system can be dynamically controlled to provide precise and accurate inlet fuel process gas stream temperatures and relative humidities, which are both essential for the efficient operation of a proton exchange membrane fuel cell over a wide range of current densities.

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BRIEF DESCRIPTION OF THE DRAWING FIGURES

For a better understanding of the present invention, and to show more clearly how it may be carried into effect, reference will now be made,

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by way of example, to the accompanying drawings, which show a preferred embodiment of the present invention and in which:

Figure 1 illustrates a schematic flow diagram of one embodiment of a humidification system for a fuel cell;

5 Figure 2 shows a perspective view of a second embodiment of the humidification system for a fuel cell;

Figure 3 shows a detail of Figure 2 in a corresponding perspective view on a larger scale;

10 Figure 4 shows a perspective view of part D of Figure 3 in a corresponding perspective view on an enlarged scale;

Figure 5 shows details of elements of a steam line;

Figure 6 shows a part of figure 5 on an enlarged scale; and

Figure 7 shows a schematic view of the humidification system of the second embodiment.

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DESCRIPTION OF THE PREFERRED EMBODIMENT

Referring first to Figure 1, this shows a schematic flow diagram of a process gas stream for one process gas. It is to be understood that the invention is applicable to both gases, i.e. to both of the fuel and the oxidant, and for this purpose the flow diagram of Figure 1 would be duplicated for the two process gas lines. The embodiments of Figure 2-6 shows the invention as applied to both process gas lines

20 Referring to Figure 1, and in that process gas stream 12 and a steam line 14 are both connected to a saturator 16, for increasing the humidity of the gas stream. Steam is supplied from a steam supply indicated schematically at 18. The saturator 16 includes an injector for injecting steam into the process gas stream, so as to both heat and humidify the process gas stream.

25 A line 20 exits from the saturator 16 and contains super-saturated process gas. The line 20 enters a first heat exchanger 22. The first heat exchanger 22 can be a plate heat exchanger or other suitable heat exchanger, and has an inlet 26 and an outlet 28 for a water stream. It is to be understood that the stream could be comprised of at least one fluid, including but not limited to water, oil, and/or ethylene glycol. While a

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variety of heat exchange fluids could be used for the specific embodiments described here, all the heat exchange fluids are water in the described embodiments. The inlet and outlet 26, 28 are part of a first temperature control circuit, also referred to as a dewpoint cooling section, including a pump 30, an inlet 32 for make-up water and a third heat exchanger 34. Additionally a first heater 36 is provided. Thus, in the first temperature control circuit, the make up water enables the level of fluid to be maintained, and this stream can be either cooled with the third heat exchanger 34 or heated with the first heater 36 to a desired temperature.

The first heat exchanger 22 has an outlet for cooled gas connected by a line 24 to a separator 38. The separator 38 is for separating water condensed out of the gas in the first heat exchanger 22, and has a discharge or outlet 40 for condensed water. An outlet of the separator 38 is connected by a further line 42 to a second heat exchanger 44.

The second heat exchanger 44 is intended to reheat the gas, and has an outlet connected to line 46 for the reheated gas. Like the first heat exchanger 22, the second heat exchanger 44 has an inlet 48 and an outlet 50 for a water heating stream. The inlet and outlet 48, 50 are part of a second temperature control circuit, also referred to as a reheating section, including a pump 52, a make-up inlet 54, a fourth heat exchanger 55, and a second heater 56. Thus, like the arrangement of the first heat exchanger 22, the pump 52 circulates the make up water, and this stream can be either cooled with the fourth heat exchanger 55 or heated with the second heater 56 to a desired temperature.

The reheated gas with the known moisture content is then passed through line 46 to the fuel cell stack indicated schematically at 60.

^{Sub B1} The arrangement of Figure 1 is intended to provide controlled humidification of the gas stream supplied to the fuel cell stack 60, and to enable both the temperature and humidity to be precisely controlled. This is explained further, by the detailed description of the mode of operation of the apparatus of Figure 1. Thus, dry incoming process is supplied to the saturator 16, and gas is super-saturated with steam in the saturator 16, to a humidity level greater than that ultimately desired for the gas. Both the

flow of the gas through line 12 and steam through line 14 are controlled and metered. The effect of injecting steam into the gas is also to heat the gas to a first pre-set temperature. Typically, on leaving the saturator 16, the gas is supersaturated at the first pre-set temperature of around 90°C, although the gas may be supersaturated at any temperature in the range of 10°C to 120°C.

In the first heat exchanger 22, the gas is cooled down to a second pre-set temperature of, for example, 80°C. Again, for example, this temperature could be in the range 10°C to 120°C. The effect of this is to remove excess moisture from the gas stream, and to give a humidity level equal to 100% relative humidity at the temperature to which the gas is cooled in the first heat exchanger 22.

The reason for first super-saturating and then cooling the gas to remove excess moisture is to ensure that the absolute humidity level is accurately achieved. Achieving a reliable humidity level in the saturator 16 is not practical. Thus, the approach has been taken of adding excess moisture and then removing excess moisture by condensation, since the absolute humidity level is known, when the gas is saturated and the dewpoint temperature of the gas is known.

The excess moisture in the gas will form droplets, and the gas with the condensed droplets is passed to the separator 38, where the condensed droplets are collected or separated from the gas flow and drained out through the outlet or discharge line 40.

The saturated gas is then passed through line 42 to the second heat exchanger 44. Here, the gas is reheated to a third pre-set temperature of, for example, 85°C. More generally, the gas can be reheated to a temperature of 10°C to 120°C. Heating the gas will reduce the relative humidity level but the absolute humidity level will remain constant.

Thus, reheated process gas from the second heat exchanger 44, passes through line 46, and it will then have a known, third pre-set temperature and a known humidity level. As indicated schematically at 58, a heater is provided to maintain the line 46 at a constant temperature, to ensure that the gas does not cool or otherwise change in temperature during passage to the fuel cell stack 60. Practically, it has been found that heat traces, comprising electrical heating wires, wound around the line 46

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provides a necessary heating function. This ensures gas delivered to fuel cell stack 60 is at the desired temperature and with the desired humidity.

Sub B2) As mentioned above, changing demands on the fuel cell stack are accomplished by changing the flow rate for the gas passing through the line 12. If it is desired to change the temperature and/or the humidity of the gas flow then this is achieved by control of the operating conditions of the first and second heat exchangers 22, 24.

Thus, the temperature of the cooling fluid in the first temperature control loop or circuit of the first heat exchanger 22, passing through the inlet and outlet 26, 28, is controlled, so as to control the temperature of gas exiting from the heat exchanger 22, and hence the absolute humidity level of this gas.

Commonly, it is expected that gas will be cooled in the first heat exchanger 22, and the second heat exchanger 44 will ensure that the cooling water passing through the cooling loop will be at a desired temperature. The third heat exchanger 34 enables the temperature in the cooling loop to be lowered quickly if desired.

Where the operational requirement is to increase the temperature of the gas exiting from the first heat exchanger 22, then the water in the cooling loop needs to be heated. For this purpose, the first heater 36 is provided to enable the water to be rapidly heated. It has been found, in practice, that response times of less than a minute can be provided for a 12kW fuel cell.

Correspondingly, in the second heat exchanger 44, the second heater 56 is adjusted to heat water in a cooling loop passing through the inlet and outlet 48 and 50 to the desired temperature. The fourth heat exchanger 55 enables the temperature in the cooling loop to be lowered quickly if desired.

Reference will now be made to Figures 2-7, which show an implementation of the present invention.

Referring to Figure 7, there is shown a schematic view of a humidification circuit according to a second embodiment. Here, a steam inlet 70 is connected to a steam supply and is provided with a pressure sensor 72, connected to a pressure switch (not shown) for tripping the fuel

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cell system. The steam supply pressure is too low. The line 70 then passes through a main shut off valve 74 and a trap 76 is provided for draining off any condensation which may have formed.

The steam line 70 then passes through a T-connection to two separate lines 90, 92 for supplying steam to the separate gas lines for the fuel and oxidant gases. Many elements of these two lines 90, 92 are common, and for simplicity, a description is given just of these elements in the line 90. The corresponding elements in the line 92 are given the same reference numeral but with a suffix "a", it being understood that they have essentially the same function.

Sub BM Thus, the line 90 includes a steam regulator or shut off valve 94 connected to a further regulating valve 96 Valve 96 is a metering valve which controls the flow of steam into the gas lines.

A fuel gas is supplied through a line 112. Steam is injected into
15 the fuel gas at an injection port 114. Steam is supplied to injection port 114
through a non-return valve 116.

The fuel gas containing steam, which is then in a supersaturated condition passes through a first heat exchanger 118, which is cooled, so as to promote condensation of excess moisture.

The cooled fuel gas then passes to a separator 120 with a trap and drain arrangement 122, for separating out also droplets. The fuel gas with 100% relative humidity then flows through a line 124, that is insulated to maintain the temperature and humidity level of the fuel gas to a second heat exchanger 126. A temperature sensor 128 is provided downstream from a separator 120, for detecting the temperature of the fuel gas stream. Knowing that the fuel gas stream will be at a 100% relative humidity, the absolute humidity of the gas stream can be determined.

From the second heat exchanger 126, the fuel gas flows to the fuel cell stack indicated at 130. Again, standard sensors can be provided as indicated at 132, immediately before the inlet to the fuel cell.

Each of the first and second heat exchangers 118, 126 has its respective temperature control circuit, and these are now described separately.

Referring first to the first heat exchanger 118, a temperature control circuit indicated at generally 132 includes a first secondary heat exchanger 134, a pump 136 and a heater 138.

Auxiliary elements of the circuit include a connection 140 for make up water and a pressure relief valve 142. Chilled cooling water is supplied to the secondary heat exchanger 134 through supply and return lines 144 and 146 with a control valve being provided at 148. A temperature sensor 150 is provided in the cooling circuit, to enable the temperature in the first heat exchanger 118 to be set as desired. Other standard control elements would be provided as required. For example, a temperature controller 152 is connected to the temperature sensor 150 and to the heater 138, and also to the control valve 148. Thus, the temperature controller 152 can open the valve 148 to increase the flow of cooling water to cool down the temperature in the circuit, or alternatively actuate the heater 138 to increase the temperature in the circuit, as required.

The temperature control circuit for the second heat exchanger 126 generally corresponds. Thus, the circuit is indicated at 162, and includes a second secondary heat exchanger 164, a pump 166 and a heater 168. A make up inlet 170 is provided, together with a pressure release valve 172.

The chilled water supply and return lines 144, 146 are connected through the second secondary heat exchanger 164, through a control valve 178.

A temperature sensor 180 is connected to the second temperature control circuit 162, and a temperature controller 182 is connected to a temperature sensor 180, control valve 178 and the heater 168, for control as for the first temperature control circuit 132.

The present invention has many advantages over the prior art. The combination of the dewpoint cooling section and the reheating section allows rapid changes in operating conditions, with typical response times which are less than one minute. Furthermore, the system can be dynamically controlled to provide precise and accurate inlet fuel process gas stream temperatures and relative humidities, which are both essential for the efficient operation of a proton exchange membrane fuel cell over a wide range of current densities.

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While the above description constitutes the preferred embodiments, it will be appreciated that the present invention is susceptible to modification and change without departing from the fair meaning of the proper scope of the accompanying claims. For example, the present invention might have applicability in other types of fuel cells, which include but are not limited to, solid oxide, alkaline, molten-carbonate, and phosphoric acid. In particular, the present invention may be applied to fuel cells which operate at much higher temperatures. As will be appreciated by those skilled in the art, the requirement for humidification is very dependent on the electrolyte used and also the temperature and pressure of operation of the fuel cell. Accordingly, it will be understood that the present invention may not be applicable to all other types of fuel cells.

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